

Heat Transfer in a Non-Newtonian Jeffery Fluid from an Inclined Vertical Plate

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Abstract

In this manuscript, the scope of implicit finite difference method in solving a mathematical model for incompressible Jeffery's fluid past an inclined vertical plate. The influence of many multi-physical parameters in these variables is illustrated graphically and skin friction and Heat transfer rate are computed and discussed through the table. The results found that fluid flow is reduced with increasing Deborah number De , but temperature is accelerates. Increasing λ enhances flow of the fluid, but temperature reduced.

Keywords: Heat Transfer, Inclined Plate, Jeffrey's Fluid, Nusselt Number, Skin Friction

1. Introduction

Non-Newtonian fluids have the emerging importance in current industries and technology, and the mathematical modelling of non-Newtonian fluid flows and their understanding are of both fundamental and practical significance. The constitutive Jeffery fluid model explained¹⁻⁶. Recently, Siva Reddy Sheri et al.,⁷ considered natural convection flow from a vertical plate in the absence of MHD with ramped temperature. Ahmad et al.,⁸ have studied mixed convection flow of a Jeffrey's non-Newtonian fluid over an exponentially stretched plate. Zin et al.,⁹ discussed the heat transfer of unsteady flow past a vertical plate under the Influence of thermal radiation and MHD. Tripathy et al.,¹⁰ explained the effects of chemical and hydromagnetic viscous flow over a vertical plate. Javed et al.,¹¹ discussed the radiation effect on MHD flow along a vertical impermeable wavy texture. Jayachandra Babu and Sandeep¹² have reported on MHD flow of Williamson fluid over a stretching sheet. Zeeshan and Majeed¹³ performed of the flow, heat transfer of Jeffery fluid past a linearly stretching sheet with the presence of a magnetic dipole. Seth¹⁴ obtained numerical solutions of the model MHD flow over semi-infinite plate through

porous regime. Most of the studies are related to vertical plate, the articles on the heat transfer in Jeffrey's flow from an inclined vertical plate are very limited. Subba Rao et al.,¹⁵ investigated non-similar solutions for the influence of thermal slipy flows of Casson viscoplastic fluid from an inclined vertical plate and he has used the Keller Box method.

Motivated by the above said research work, in the present paper, we investigate a numerical solution for two dimensional incompressible viscoelastic Jeffrey's non-Newtonian fluid flow from an inclined vertical plate. Numerical solutions for the velocity and the temperature are obtained using a powerful technique namely finite difference method (Keller-Box).

2. Mathematical Model

We examine steady buoyancy-driven convection flow of Jeffrey's non-Newtonian fluid over an inclined vertical plate. Figure 1 shows the flow model and associated coordinate system. The x - axis taken along the cone surface measured from the origin and the y - axis is measured normal to the surface.

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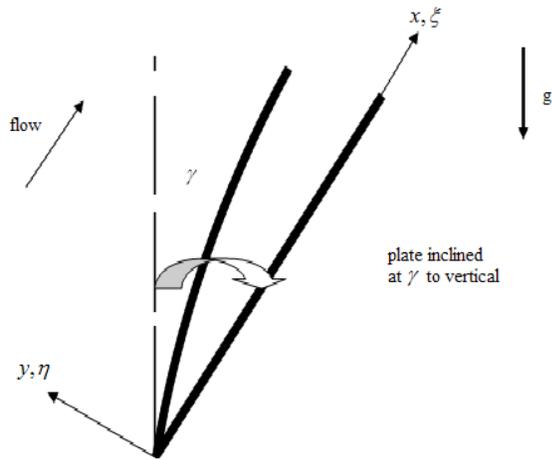


Figure 1. Non-Newtonian heat transfer over a plate.

For an incompressible Jeffrey’s fluid, the continuity, momentum and energy equations are:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\nu}{1+\lambda} \left[\frac{\partial^2 u}{\partial y^2} + \lambda_1 \left(u \frac{\partial^3 u}{\partial x \partial y^2} - \frac{\partial u}{\partial x} \frac{\partial^2 u}{\partial y^2} + \frac{\partial u}{\partial y} \frac{\partial^2 u}{\partial x \partial y} + v \frac{\partial^3 u}{\partial y^3} \right) \right] + g\beta(T - T_\infty) \cos \gamma \tag{2}$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \frac{\partial^2 T}{\partial y^2} \tag{3}$$

The following spatial and temporal boundary conditions:

At $x = 0, u = u_\infty, T = T_\infty$

At $y = 0, u = 0, v = 0, T = T_w$ (4)

As $y \rightarrow \infty, u \rightarrow u_\infty, T = T_\infty$

Taking the following non-dimensional quantities:

$$\eta = y \left(\frac{u_\infty}{\nu x} \right)^{1/2}, \xi = \xi(x), f(\xi, x) = \frac{\psi(x, y)}{(\nu u_\infty x)^{1/2}}, \theta(\xi, x) = \frac{(T - T_\infty)}{(T_w - T_\infty)}$$

$$Gr = \frac{g\beta(T_w - T_\infty)x^3}{\nu^2}, De = \frac{\lambda_1 U_\infty}{x}, Pr = \frac{\nu}{\alpha}, Re_x = \frac{U_\infty x}{\nu} \tag{5}$$

Here $u = \frac{\partial \psi}{\partial y}$ and $v = -\frac{\partial \psi}{\partial x}$ are the velocity components in the x - and y - directions respectively, ψ -stream function, $\nu = \mu / \rho$ - the kinematic viscosity of the conducting fluid, k - the thermal conductivity, γ - inclination of the plate to the vertical, De - Deborah

number, λ - the ratio of relaxation to retardation times, λ_1 - the retardation time. Pr - Prandtl number, Gr - Grashof number, T_∞ - the free stream temperature, Re_x - Local Reynolds number, $\xi = Gr / Re_x^2$ - thermal buoyancy force parameter for forced convection.

In view of Eqs (5) the governing equations (2)-(3) and dropping primes yields the following dimensionless equations:

$$\frac{1}{1+\lambda} f''' + \frac{1}{2} f f'' - \frac{De}{1+\lambda} \left(f f''' + \frac{1}{2} f''^2 - \frac{1}{2} f f^{iv} \right) + \xi \theta \cos \gamma = \xi \left(f' \frac{\partial f'}{\partial \xi} - f'' \frac{\partial f}{\partial \xi} - \frac{De}{1+\lambda} \left(f' \frac{\partial f''}{\partial \xi} - f''' \frac{\partial f'}{\partial \xi} + f'' \frac{\partial f''}{\partial \xi} - f^{iv} \frac{\partial f}{\partial \xi} \right) \right) \tag{6}$$

$$\frac{\theta''}{Pr} + \frac{1}{2} f \theta' = \xi \left(f' \frac{\partial \theta}{\partial \xi} - \theta' \frac{\partial f}{\partial \xi} \right) \tag{7}$$

The dimensionless form of the boundary conditions:

At $\eta = 0, f = 0, f' = 0, \theta = 1$

As $\eta \rightarrow \infty, f' = 1, \theta = 0$ (8)

The Skin friction coefficient and Nusselt number in the non-dimensional form is given by

$$\frac{1}{2} C_f Re_x^{-1/2} = f''(\xi, 0) \tag{9}$$

$$\frac{Nu}{\sqrt{Re_x}} = -\theta'(\xi, 0) \tag{10}$$

3. Computational Finite Difference Solutions

The finite difference method (Keller-Box) is employed to solve the transformed, coupled boundary layer problem defined by eqns. (6)-(7) under (8). Keller-Box method is the most versatile technique available for engineering analysis and equally adept at handling ordinary or partial differential equations as well as integral equations. Keller box method was originally settled for low speed aerodynamic problems and this system is established by Keller¹⁶. These include Casson slip boundary layer flows¹⁷. This method remains among the most powerful, versatile and accurate computational finite difference schemes employed in modern viscous fluid dynamics simulations. This method has been used extensively and effectively for over three decades in a large spectrum of nonlinear fluid mechanics problems. Keller’s method

provides unconditional stability and rapid convergence for strongly non-linear flows.

4. Results and Interpretation

The nonlinear boundary value problem solved in the previous section is dictated by an extensive number of thermal and hydrodynamic parameters. In order to gain a clear insight into the physical problem, numerical calculations for distribution of the velocity and temperature for different values of these parameters is conducted with graphical illustrations (Figure 2–4). For the purpose of our computation, we adopted the following default parameters: $Pr = 0.71, De = 0.1, \lambda = 0.2, \xi = 1.0, \gamma = 70^\circ$ are initial values (unless otherwise stated). Table 1 shows that the effects of Deborah number De and λ on skin friction, Nusselt number, along with a difference in oblique coordinate, ξ . With increasing De , the Nusselt number (heat transfer rate) increases significantly and

skin friction is reduced. A rising effect in λ is observed that enhance skin friction and Nusselt number.

In Figures 2(a)-2(b), present the evolution in the effect of the ratio of relaxation to retardation times i.e. λ on the velocity (f') and temperature (θ). Fluid flow is significantly increased with increasing λ . Conversely temperature is depressed slightly with increasing values of λ . In Figures 3(a)-3(b), illustrate the velocity (f') and temperature (θ) with a difference in Deborah number (De). Velocity component of the fluid flow (Figure 3a) is considerably reduced with increasing De . In Figure 2b, an increase Deborah number is seen to considerably enhance temperature all the way through the surface of plate. Figure 4(a)-4(b) presents the influence of the plate inclination on the dimensionless velocity and temperature. Taking angle of the plate ($\gamma < 0$) i.e. negative inclination, in Figure 4a, the velocity is reduced. Conversely in Figure 4b, with $\gamma < 0$ negative inclination the temperature decreases slightly. Further, more temperatures are improved marginally with positive inclination of the plate.

Table 1. Values of $f''(\xi, 0)$ and $-\theta'(\xi, 0)$ for different ξ , De , and λ

De	λ	$\xi = 1.0$		$\xi = 2.0$		$\xi = 3.0$	
		$f''(\xi, 0)$	$-\theta'(\xi, 0)$	$f''(\xi, 0)$	$-\theta'(\xi, 0)$	$f''(\xi, 0)$	$-\theta'(\xi, 0)$
0.5	0.2	0.4040	0.3133	0.8956	0.3205	1.4699	0.3270
		0.3977	0.3164	0.8844	0.3234	1.4546	0.3298
		0.3864	0.3232	0.8645	0.3298	1.4241	0.3357
1.0	0.0	0.3725	0.3029	0.8223	0.3100	1.3446	0.3165
	1.0	0.5337	0.3332	1.1887	0.3413	1.9573	0.3485
	2.0	0.6583	0.3505	1.4732	0.3589	2.4348	0.3664

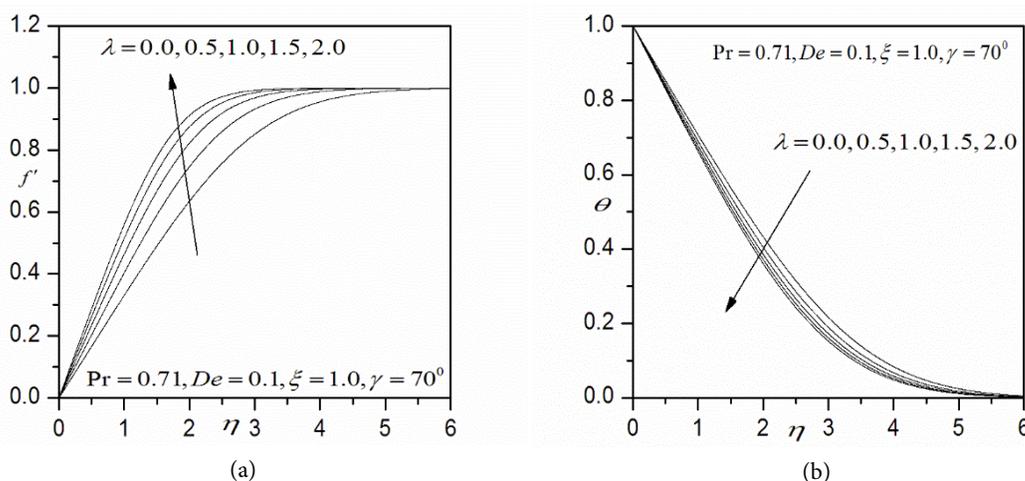


Figure 2. (a) Influence of λ on velocity profiles. (b) Influence of λ on temperature profiles.

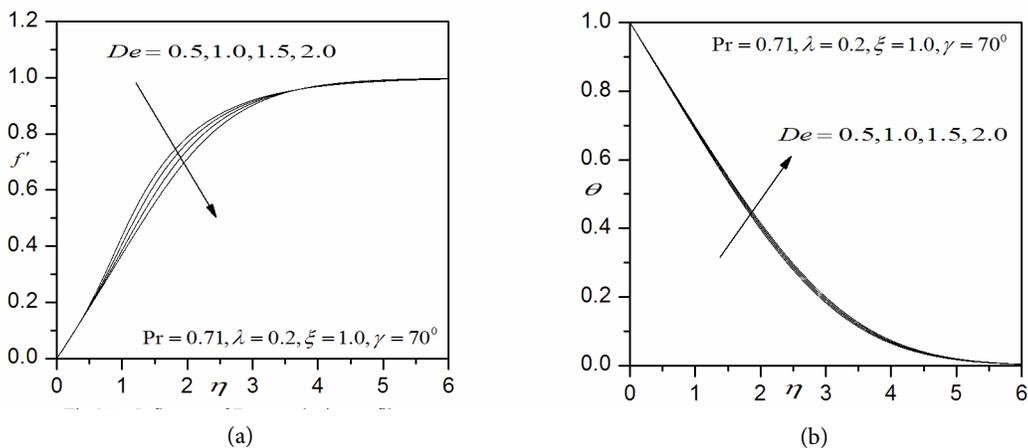


Figure 3. (a) Influence of De on velocity profiles. (b) Influence of De on temperature profiles.

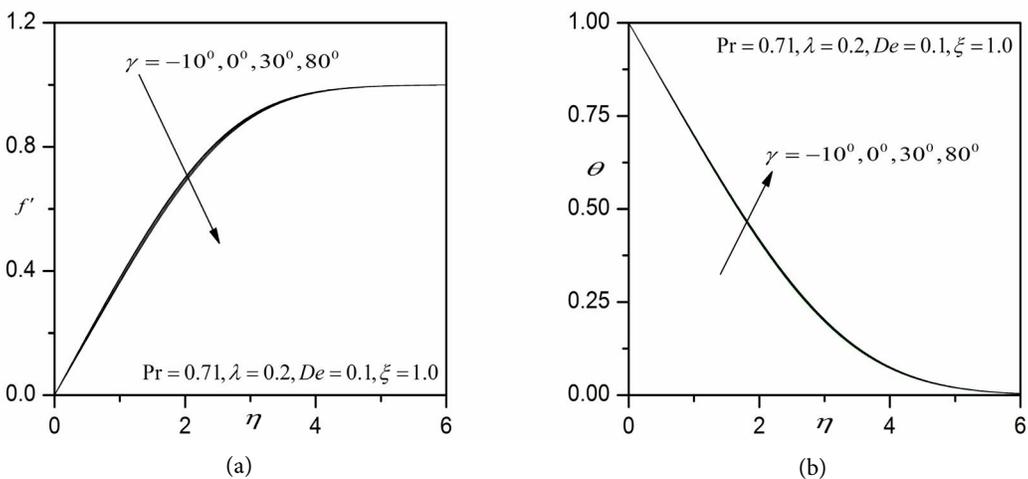


Figure 4. (a) Influence of γ on velocity profiles. (b) Influence of γ on temperature profiles.

5. Conclusion

In this work, motivated by applications in non-Newtonian fluid model has been developed for *heat transfer of Jeffery’s fluid from an inclined vertical plate*. The governing equations are solved numerically the finite difference method. Numerical results are reported for various values selected parameters interest. When De takes the values larger than 0.5, the flow near plate decreases, skin friction- $f''(\xi, 0)$ and heat transfer rate $(-\theta'(\xi, 0))$ while enhances temperature. Raising the parameter ratio of relaxation and retardation times (λ), hike the velocity, skin friction coefficient $f''(\xi, 0)$, heat transfer rate $(-\theta'(\xi, 0))$ it reduces whereas temperature for all values of radial coordinate.

6. References

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